

Pressure Loss in Pipelines

Sample document with complete example values. It shows the report the purchased export produces for YOUR input - it is not itself a report for any part.

Project: Sample project

Part/Position: no real part

Prepared by: Sample, not released

Velocity assessment: within guideline

Medium

Medium Wasser 20 °C
Density ρ 998.2 kg/m³
Kinematic viscosity ν 1.004 mm²/s

Pipe and Geometry

Material Stahl nahtlos neu
Nominal diameter DN50
Inside diameter d 50 mm
Pipe length L 20 m
Roughness k 0.045 mm
Relative roughness k/d 0.0009

Flow

Volumetric flow rate V 14.137 m³/h
Velocity v_{bar} 2 m/s
Reynolds number Re 99,602
Flow regime turbulent
Pipe friction factor λ 0.0218
 λ method Colebrook-White (iterated)
 λ comparison, Colebrook 0.0218
 λ comparison, Haaland 0.0216
 λ comparison, Swamee-Jain 0.022
Dynamic pressure p_{dyn} 1,996 Pa

Fittings and local losses

ζ value	Count	$n \cdot \zeta$
0.5	1	0.5
0.3	4	1.2
0.2	2	0.4
1	1	1

Fittings and local losses

Sum $\Sigma \zeta$ 3.1
Equivalent length L_{eq} 7.1 m

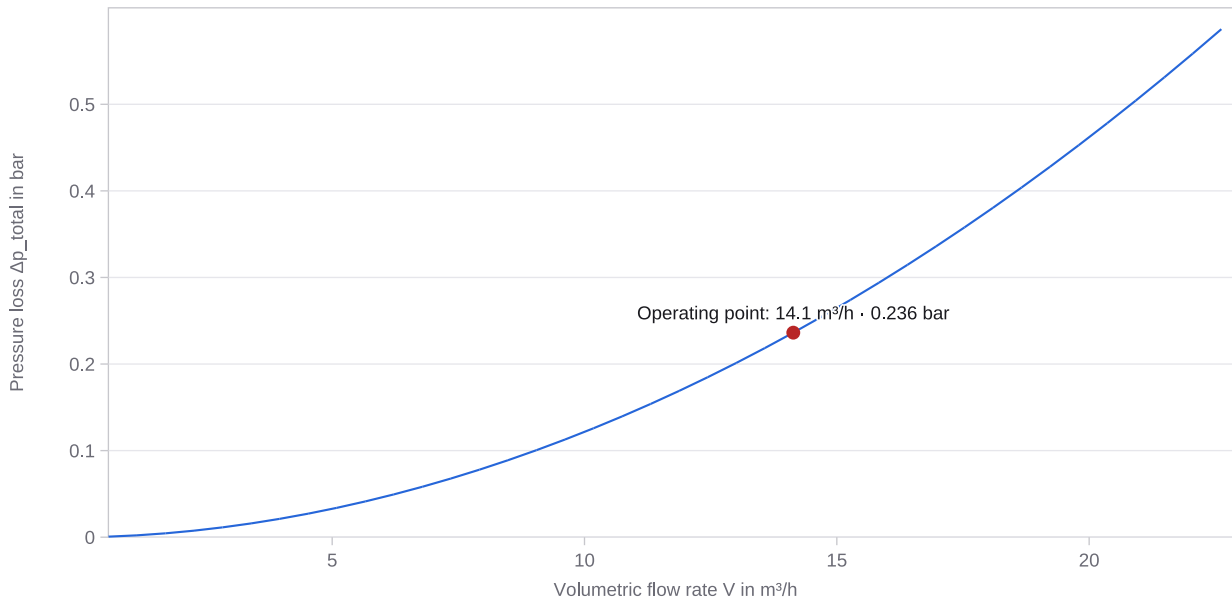
Result: Pressure Loss Components

Component	Pa	bar	m head
Pipe friction	17,435	0.1743	1.78
Fittings and local losses	6,189	0.0619	0.632
Elevation	0	0	0
Total	23,623	0.2362	2.412

Flow Velocity Assessment

Criterion	Value	Limit	Status
Velocity v_{bar} (application recommendation)	2 m/s	1 ... 2 m/s	● OK

System curve Δp over volumetric flow rate



Notes and Calculation Basis

Friction loss per Darcy-Weisbach $\Delta p = \lambda \cdot (L/d) \cdot (\rho/2) \cdot v_{\text{bar}}^2$, local losses via the ζ method $\Delta p = \sum \zeta \cdot (\rho/2) \cdot v_{\text{bar}}^2$, elevation component $\rho \cdot g \cdot \Delta z$. The pipe friction factor λ follows laminar exactly from $64/\text{Re}$, turbulent from Colebrook-White (iterated); Haaland and Swamee-Jain serve as a comparison.

Roughness values, ζ values and recommended velocities are reference values with real-world scatter (manufacturing, ageing, scaling); manufacturer data takes precedence. Model: steady, incompressible, fully developed flow in a full circular pipe - not a complete engineering verification.

About this sample

All values on these pages come from a freely chosen example calculation and belong to no real part. The purchased export contains the same sections with your input, your header data (project, part, prepared by) and as searchable text. Pricing and scope: maschinenbaurechner.de/en/pricing

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